Epoxidation of Alkenes with O<sub>2</sub> Catalyzed by EuCl<sub>3</sub> under Ambient Conditions

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EuCl3 dissolved in a mixture of propanoic acid and 1,2-dichloroethane catalyzed the epoxidation of 1-hexene (81.4% selectivity, 5.34% yield for 1 h) with O2 in the presence of Zn powder at 40 °C. The epoxidation was also catalyzed by LaCl3 (0.75% yield) and SmCl3 (0.57% yield), but CeCl3 (0.08% yield) was inactive. Epoxidations of styrene and cyclohexene were also promoted by the EuCl3-catalytic system.

We have very recently reported that the rare earth salts catalyze the partial oxidation of alkanes (hexane, cyclohexane, and adamantane) with O<sub>2</sub> in the liquid phase at ambient temperature.<sup>1)</sup> EuCl<sub>3</sub> was the most active catalyst for the mono-oxygenation of alkanes among the rare earth salts tested. In this work, we report that the same catalytic systems are also suitable for epoxidation of alkanes as shown in Scheme 1.

A simple, one-step synthesis of epoxides is one of the most attractive themes for the researchers in academic fields as well as in chemical industry. Some reaction systems for the epoxidations with O<sub>2</sub> using transition metal complexes were reported.<sup>2</sup>, <sup>3</sup>) However, it is desired to develop a new catalytic system for one-step epoxidation of alkenes with O<sub>2</sub> under mild conditions. Our reaction system was catalyzed by a simple rare earth salt such as chloride. Components of our reaction system are resemble to those of the Gif-Orsay-Texas system,<sup>4</sup>) except for solvent (CH<sub>2</sub>Cl<sub>2</sub>) and catalyst (EuCl<sub>3</sub>). However, the epoxidation of 1-hexene does not proceed in the Gif-Orsay-Texas system.

Table 1 shows experimental results for the epoxidation of 1-hexene catalyzed by some rare earth salts at 40 °C for 1 h. The standard procedure for the epoxidation was as follows. Rare earth salt of 30  $\mu$ mol was dissolved in a mixed-solution of acetic acid (2 ml) as a proton donor, dichloromethane (2 ml) as a solvent in a three-necked flask with a reflux condenser. After 1-hexene (1 ml) and Zn powder (1 g) as an electron donor had been added to the solution, the reaction was started by stirring the solution and slurry under a stream of O2 as an oxidant (10 ml•min<sup>-1</sup> at 1 atm). The products were extracted from the crude reaction mixture and were analyzed by GC-technique. The yields of products were evaluated on the basis of the 1-hexene converted. Fairly good yields of epoxide were observed for most of rare earth salts shown in Table 1, but catalytic activities for Eu2(SO<sub>4</sub>)<sub>2</sub>, EuF<sub>3</sub> and CeCl<sub>3</sub> were quite low. The yield of the epoxide for EuCl<sub>3</sub> was the highest among the rare earth catalysts tested. The products other than 1,2-epoxyhexane were 1-hexanal, 1,2-hexane-diol,

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Catalyst	Yield of epoxide / %	Selectivity to epoxide / %	TON b)
LaCl <sub>3</sub>	0.75	74.0	2.7
CeCl <sub>3</sub>	0.08	55.8	0.4
SmCl <sub>3</sub>	0.57	73.3	2.1
EuCl <sub>3</sub>	3.39	65.8	13.8
Eu(NO <sub>3</sub> ) <sub>3</sub>	2.25	67.1	8.9
Eu <sub>2</sub> (CO <sub>3</sub> ) <sub>3</sub>	1.76	73.9	6.3
Eu(CH <sub>3</sub> COO) <sub>3</sub>	1.19	61.1	5.2
Eu(ClO <sub>4</sub> ) <sub>3</sub>	0.77	38.2	5.4
Eu <sub>2</sub> (SO <sub>4</sub> ) <sub>3</sub>	0.20	62.7	0.8
EuF <sub>3</sub>	0.16	65.2	0.7
blank	0.06	50.1	-

a) Reaction temperature was 40  $^{\circ}$ C, reaction time 1 h, rare earth salts 30  $\mu$ mol,

1-hexene-3-ol, 1-hexanol, 2-hexanol, some C6 oxygenates and CO<sub>2</sub>. The formation of CO<sub>2</sub> of 35  $\mu$ mol was detected in the gas phase during the epoxidation using EuCl<sub>3</sub> catalyst. The selectivity to the epoxide for LaCl<sub>3</sub> was the highest and that for EuCl<sub>3</sub> was fairly good. The order of TON (turn over number for total amount of the products) was EuCl<sub>3</sub> > Eu(NO<sub>3</sub>)<sub>3</sub> > Eu<sub>2</sub>(CO<sub>3</sub>)<sub>3</sub> > Eu(ClO<sub>4</sub>)<sub>3</sub> > Eu(CH<sub>3</sub>COO)<sub>3</sub> > LaCl<sub>3</sub> > SmCl<sub>3</sub> > Eu<sub>2</sub>(SO<sub>4</sub>)<sub>3</sub> > EuF<sub>3</sub>> CeCl<sub>3</sub> ≈ blank. EuCl<sub>3</sub> is the most active catalyst for the oxidation of 1-hexene. These orders for catalytic activities were true also for the oxidation of cyclohexane. 1)

Table 2 shows the effects of some solvents on the epoxidation using EuCl<sub>3</sub>. When solvents of 1,2-dichloroethane, dichloromethane, acetone, diethyl ether were used for the epoxidation, the yields of the epoxide became larger than that without solvent, and the selectivities and the TON were improved. The maximum yield (4.38%) was obtained when 1,2-dichloroethane was used. Thus, 1,2-dichloroethane was the most suitable solvent for the epoxidation of 1-hexene.

Effects of some carboxylic acids on the epoxidation were also examined using dichloromethane, as shown in Table 3. The order of the yields of the epoxide obtained for the acids was acetic acid = propanoic acid > butyric acid > isobutyric acid >> trifluoroacetic acid. In the case of trifluoroacetic acid, the epoxide was not produced, but 1-hexanal (1.19% yield) and 1-hexene-3-al (0.78% yield) were obtained as the major products. The selectivity to the epoxide was improved by using butyric acid and propanoic acid, which were larger than

<sup>1-</sup>hexene 1 ml, CH<sub>3</sub>COOH 2 ml, CH<sub>2</sub>Cl<sub>2</sub> 2 ml, Zn powder 1 g, and O<sub>2</sub> 10 ml•min-1 at 1 atm.

b) Turn over number for the sum amount of the products.

Table 2.	Effect of sol	vents for the	epoxidation of	of 1-hexene	catalyzed by	EuCl <sub>2</sub> a)

Solvent	Yield of epoxide / %	Selectivity to epoxide / %	TON <sup>a)</sup>
CH <sub>2</sub> Cl <sub>2</sub>	3.38	65.8	13.8
$(CH_2Cl)_2$	4.38	74.2	15.7
$(CH_3)_2CO$	2.84	66.7	11.4
$(C_2H_5)_2O$	1.44	70.0	5.5
CH <sub>3</sub> CN	1.10	48.7	6.0
$C_5H_5N$	0.03	5.9	1.3
without	1.23	52.2	6.3

a) Reaction temperature was 40 °C, reaction time 1 h, EuCl<sub>3</sub> 30  $\mu$ mol, 1-hexene 1 ml, CH<sub>3</sub>COOH 2 ml, solvent 2 ml, Zn powder 1 g, O<sub>2</sub> 10 ml•min-1 at 1 atm.

Table 3. Effect of carboxylic acids for the epoxidation of 1-hexene catalyzed by EuCl<sub>3</sub>a)

Carboxyric acid	Yield of epoxide / %	Selectivity to epoxide / %	TON b)
CH <sub>3</sub> COOH	3.38	65.8	13.8
C <sub>2</sub> H <sub>5</sub> COOH	3.34	77.1	11.6
C <sub>3</sub> H <sub>7</sub> COOH	2.15	80.6	7.1
(CH <sub>3</sub> ) <sub>2</sub> CHCOOH	0.57	58.3	2.6
CF <sub>3</sub> COOH	0	0	7.0

a) Reaction temperature was 40  $^{\circ}$ C, reaction time 1 h, EuCl<sub>3</sub> 30  $\mu$ mol, 1-hexene 1 ml, carboxylic acid 2 ml, CH<sub>2</sub>Cl<sub>2</sub> 2 ml, Zn powder 1 g, O<sub>2</sub> 10 ml $^{\bullet}$ min<sup>-1</sup> at 1 atm.

that for acetic acid. Thus, a good yield to the epoxide was obtained by using of propanoic acid. This result was also different from that obtained for the oxidation of cyclohexane, i.e., the product yield in the case of propanoic acid was less than 40 % of that for acetic acid.1)

As described above, the most suitable solvents and carboxylic acids for the epoxidation of 1-hexene ((CH<sub>2</sub>Cl)<sub>2</sub>, C<sub>2</sub>H<sub>5</sub>COOH) were different from those for the oxidation of cyclohexane (CH<sub>2</sub>Cl<sub>2</sub>, CH<sub>3</sub>COOH). When 1,2-dichloroethane and propanoic acid were used for the epoxidation of 1-hexene, the maximum yield of 5.34% and TON of 17.6 were obtained in the present work.

b) Turn over number for the total amount of the products.

b) Turn over number for the total amount of the products.

In order to get information for the active oxygen species generated on EuCl<sub>3</sub>-system, the epoxidations of more reactive alkenes (styrene and cyclohexene) than 1-hexene were carried out under the standard reaction conditions. Epoxidation of styrene to styrene oxide proceeded as shown in Table 4, but the selectivity to styrene oxide was fairly low compared with that observed for 1-hexene. The selectivities to benzyl alcohol (33%) and benzaldehyde (28%) were greater than that to the epoxide. Acetophenone (14% selectivity) and phenyl acetaldehyde (7% selectivity) were also produced. When the reaction temperature decreased to 10 °C from 40 °C (standard conditions), the selectivity to styrene oxide increased up to 38%. However, the selectivity to the sum of benzyl alcohol and benzaldehyde (50%) was fairly high at 10 °C. Oxidation of cyclohexene by EuCl<sub>3</sub> catalyst also proceeded under the standard conditions. The selectivity to cyclohexene oxide was low comared with that observed for 1-hexene. Main product was cyclohexanone (28% selectivity) and other major products were 2cyclohexene-1-ol (11% selectivity) and 2-cyclohexene-1-one (10% selectivity). The active oxygen species generated in the catalytic system of EuCl<sub>3</sub> was so reactive as to oxidize C-H bond of alkanes. 1) Thus, it is not surprising that two allyl positions of cyclohexene have been easily oxidized. As described above, reactivity of the active oxygen species generated in the catalytic system in this work must be so strong for reactive alkenes that the selective epoxidations do not occur.

Further investigations are needed to clarify the nature of the active oxygen species generated in the EuCl<sub>3</sub> system, LaCl<sub>3</sub> system and SmCl<sub>3</sub> system.

Reactant	Yield of epoxide /%	Selectivity to epoxide /%	TON b)
styrene	0.33	15.6	6.1
cyclohexene	1.40	23.8	19.2

Table 4. Epoxidation of styrene and cyclohexene with O<sub>2</sub> catalyzed by EuCl<sub>3</sub><sup>a)</sup>

## References

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a) Reaction temperature was 40 °C, reaction time 1 h, EuCl<sub>3</sub> 30  $\mu$ mol, alkene 1 ml, CH<sub>3</sub>COOH 2 ml, CH<sub>2</sub>Cl<sub>2</sub> 2 ml, Zn powder 1 g, O<sub>2</sub> 10 ml•min<sup>-1</sup> at 1 atm.

b) Turn over number of EuCl<sub>3</sub> for the total amount of the products.